

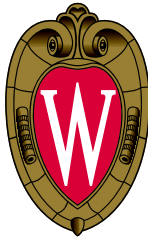
# Cyclus Fuel Cycle Simulation Capabilities with the Cyder Disposal System Model

Global 2013

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# Outline

## 1 Motivation

Future Fuel Cycle Options  
Geologic Disposal Concept Options  
Fuel Cycle Simulator Capabilities

## 2 Modeling Capabilities

Cyber Overview  
Radionuclide Transport in Cyber  
Thermal Transport in Cyber

## 3 Conclusion





# Future Fuel Cycle Options

**Domestic Fuel Cycle Options**

Title	Description	Challenges
Open	Once Through Current US PWR Fleet No Separations No Recycling Higher Burnups	High Temperatures, Volumes
Modified Open	Partial Recycling Next Gen. PWR Fleet Limited Separations Limited Transmutation Advanced Fuel Forms HLW treatment	Both high volumes and variable spent fuel streams
Closed	Full Recycling Full Separations Full Recycling VHTGR, SFRs, other transmutation HLW treatment	Variable spent fuel streams

**Table 1 : Domestic Fuel Cycle Options**



## Disposal Geology Options Considered

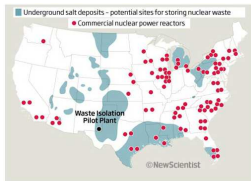


Figure 1 : U.S. Salt Deposits, ref. [26].

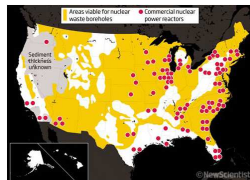


Figure 3 : U.S. Crystalline Basement, ref. [26].



Figure 2 : U.S. Clay Deposits, ref. [11].



Figure 4 : U.S. Granite Beds, ref. [6].



## Cyclus Top Level Fuel Cycle Simulator

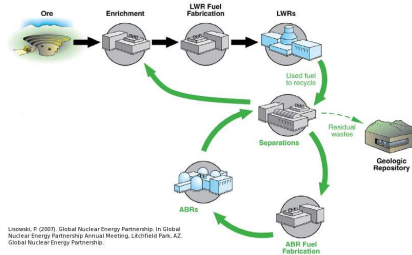


Figure 5 : Top level simulators are intended to model the collective behavior of various fuel cycle decisions and strategies [24].



Figure 6 : [cyclus.github.com](https://cyclus.github.com) [17].



## Need For an Integrated Repository Model

**Repository Capabilities within Systems Analysis Tools**

Tool	Institution	Fuel Disposition	Radionuclide Transport	Heat Transport
NUWASTE[2]	NWTRB	yes	no	no
VISION [38]	INL	yes	no	YMR only
DANESS [34]	ANL	no	no	no
COSI [3]	CEA	yes	no	yes
NFCSim [31]	LANL	no	no	no
CAFCA [14]	MIT	no	no	no
ORION [14]	BNL	no	no	no
TSM [33]	OCRWM	yes	no	YMR only

**Table 2 :** System tools are lacking in radionuclide transport and heat transport calculations in generic geologic media.

## Contributions from This Work



This work has provided a platform capable of bridging the gap between fuel cycle simulation and repository performance analysis.

- Conducted thermal transport sensitivity analyses. [19, 18]
- Conducted contaminant transport sensitivity analyses. [20]
- CYDER achieved integration with a fuel cycle simulator.
- Abstracted physical models of thermal and contaminant transport. [22]
- Demonstrated dominant physics of those models in CYDER, integrated with CYCLUS. [23, 17]
- Published source code, documentation, and testing to facilitate extension by external developers. [21]



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Thermal Transport in Cyder

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## Cyder Paradigm : Waste Stream Acceptance

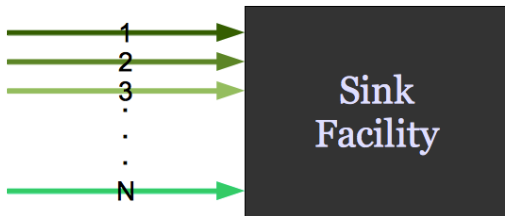
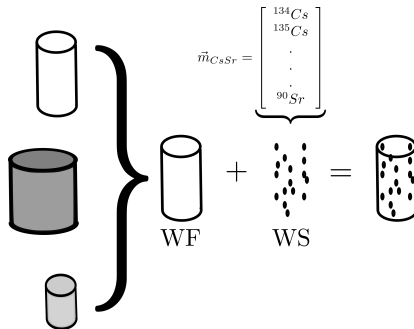


Figure 7 : To participate in a CYCLUS fuel cycle simulation, CYDER must accept **arbitrary** spent fuel and high level waste **material data objects**.



## Cyder Paradigm : Waste Stream Conditioning

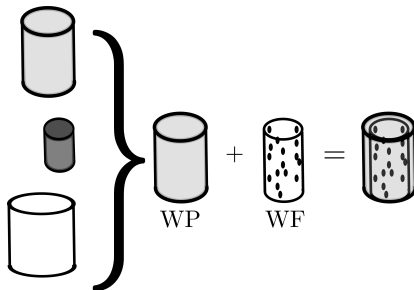


**Figure 8 :** In Cyder, discrete waste streams are conditioned into the appropriate discrete waste form according to user-specified pairings.





## Cyber Paradigm : Waste Form Packaging

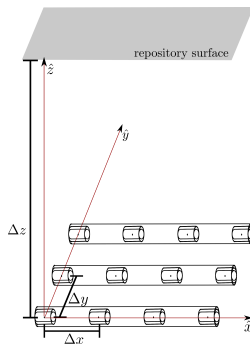


**Figure 9 :** In Cyder, one or more waste forms are loaded into the appropriate waste package according to user-specified pairings.



## Cyber Paradigm : Waste Package Emplacement

Finally, the waste package is **emplaced** in a buffer component, which contains many other waste packages, spaced evenly in a grid. The grid is defined by the user input and depends on repository depth,  $\Delta z$ , waste package spacing,  $\Delta x$ , and tunnel spacing,  $\Delta y$  as in Figure 10.

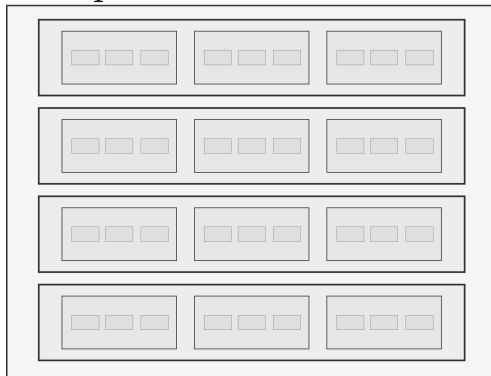


**Figure 10 :** The repository layout has a depth and a uniform package spacing.

## Cyder Paradigm : Modularity



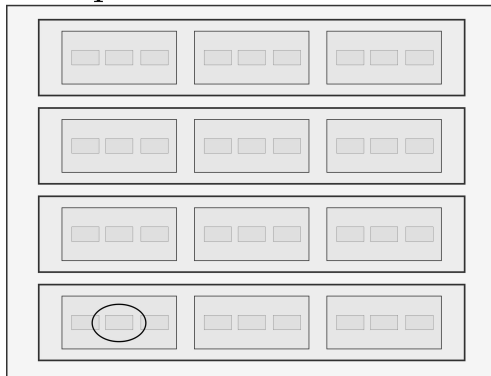
### Components



## Cyder Paradigm : Modularity

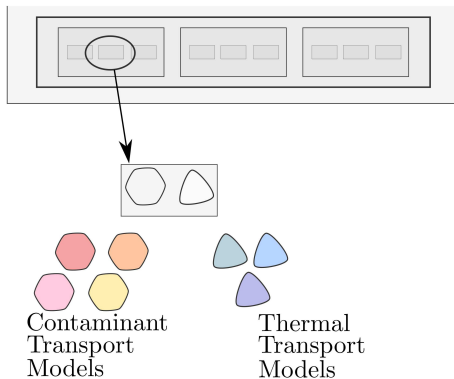


### Components





## Cyder Paradigm : Modularity





## Clay GDSM Sensitivity Analysis

- Barrier Degradation
- Sorption
- Solubility
- Advective Velocity
- Diffusivity

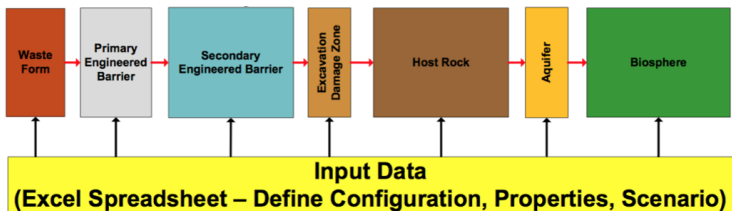


Figure 11 : The Clay Generic Disposal System Model (GDSM) was used for preliminary sensitivity analysis, abstraction iteration, and validation. This figure was reproduced from Figure 3.3-2 in [9].



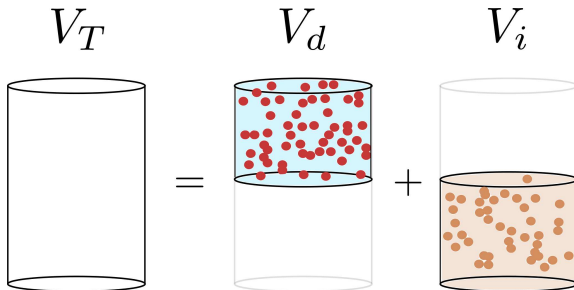
## Nested Components

The NuclideModel in a Component can be interchangeably represented by any of the four nuclide transport models.

- Degradation Rate Based Failure Model
- Mixed Cell with Degradation, Sorption, Solubility Limitation
- Lumped Parameter Model
- 1 Dimensional Approximate Advection Dispersion Solution, Brenner [4]



## Radionuclide Transport: Degradation Rate Based Release

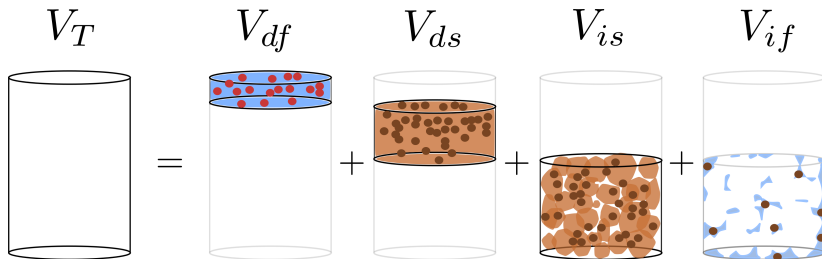


**Figure 12 :** The control volume contains an intact volume  $V_i$  and a degraded volume,  $V_d$ . Contaminants in  $V_d$  are available for transport, while contaminants in  $V_i$  are contained.





## Radionuclide Transport : Mixed Cell with Sorption and Solubility



**Figure 13 :** The degraded volume is modeled as a solid degraded volume,  $V_{ds}$ , and a fluid degraded volume,  $V_{df}$ . The intact volume is modeled as an intact solid volume,  $V_{is}$ , and an intact fluid volume  $V_{if}$ . Only contaminants in  $V_{df}$  are available for transport.



## Radionuclide Transport : Mixed Cell Sorption

The mass of contaminant sorbed into the degraded and precipitated solids can be found using a linear isotherm model [32], characterized by the relationship

$$s_i = K_{di} C_i \quad (1)$$

where

$s_i$  = the solid concentration of isotope  $i$  [ $kg/kg$ ]

$K_{di}$  = the distribution coefficient of isotope  $i$  [ $m^3/kg$ ]

$C_i$  = the liquid concentration of isotope  $i$  [ $kg/m^3$ ].



## Radionuclide Transport : Mixed Cell Solubility Limitation

In addition to engineered barriers, contaminant transport is constrained by the solubility limit [16],

$$m_{s,i} \leq V_w C_{sol,i}, \quad (2)$$

where

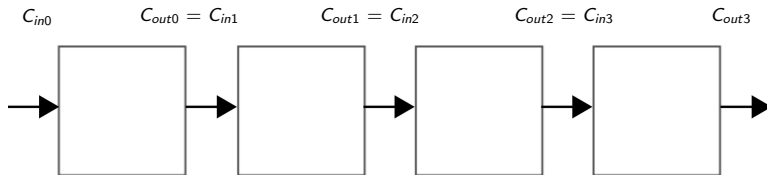
$m_{s,i}$  = solubility limited mass of isotope  $i$  in volume  $V_w$  [kg]

$V_w$  = volume of the solution [ $m^3$ ]

$C_{sol,i}$  = solubility limit, the maximum concentration of  $i$  [ $kg/m^3$ ].



## Radionuclide Transport: Lumped Parameter Transport Model



**Figure 14 :** The method by which each lumped parameter component is modeled is according to a relationship between the incoming concentration,  $C_{in}(t)$ , and the outgoing concentration,  $C_{out}(t)$ .

$$C_{out}(t) = \int_0^{\infty} C_{in}(t - t')g(t')e^{-\lambda t'} dt' \quad (3)$$

where

$t'$  = time of entry [s]

$t - t'$  = transit time [s]

$g(t - t')$  = response function, a.k.a. transit time distribution[-]

$\lambda$  = radioactive decay constant[s<sup>-1</sup>].



## Radionuclide Transport: 1D Finite, Cauchy B.C.

$$-D \frac{\partial C}{\partial z} \Big|_{z=0} + vC = \begin{cases} vC_0 & t < t_0 \\ 0 & t > t_0 \end{cases} \quad \frac{\partial C}{\partial z} \Big|_L = 0$$

**Figure 15 :** A one dimensional, finite, unidirectional flow, solution with Cauchy and Neumann boundary conditions [35, 4].



# Clay GDSM Degradation Rate Sensitivity

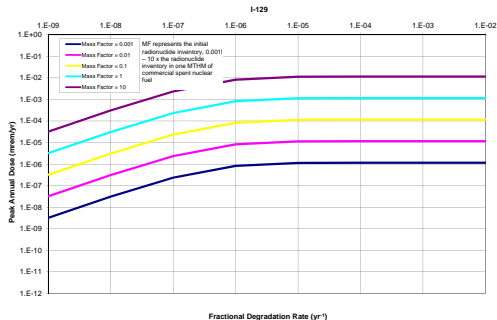


Figure 16 : <sup>129</sup>I waste form degradation rate sensitivity.



## Cyder Degradation Rate Sensitivity

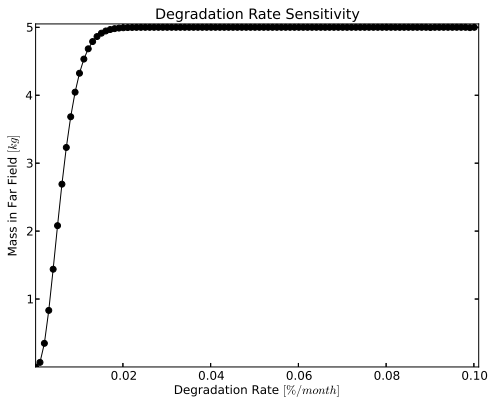
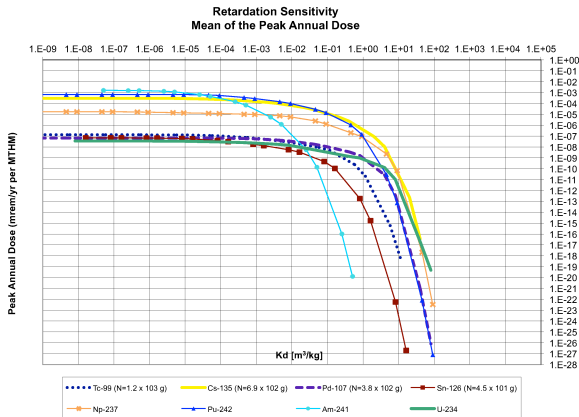


Figure 17 : Sensitivity demonstration of the degradation rate in CYDER for an arbitrary isotope.



# Clay GDSM Sorption Sensitivity



**Figure 18 :**  $K_d$  sensitivity. The peak annual dose due to an inventory,  $N$ , of each isotope.





## Cyder Sorption Sensitivity

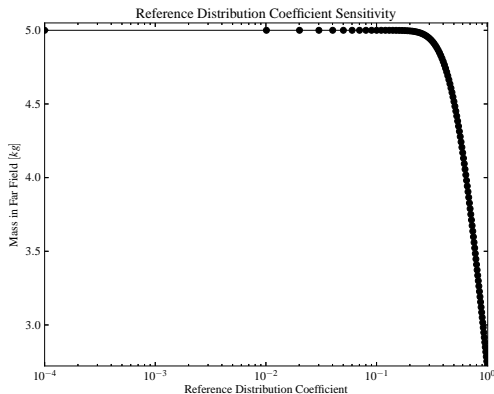
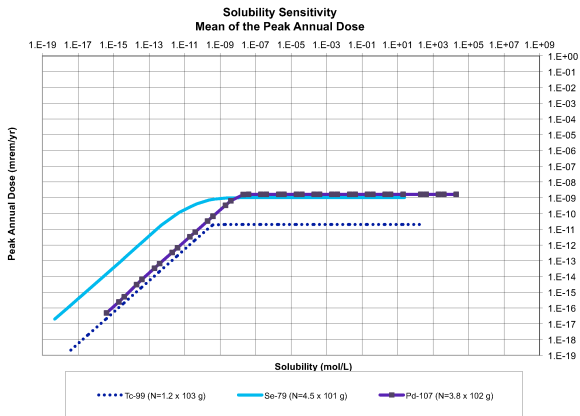


Figure 19 :  $K_d$  factor sensitivity in the CYDER tool for an arbitrary isotope assigned a variable  $K_d$  coefficient.



## Clay GDSM Solubility Sensitivity



**Figure 20 :** Solubility limit sensitivity. The peak annual dose due to an inventory,  $N$ , of each isotope.



## Cyder Solubility Sensitivity

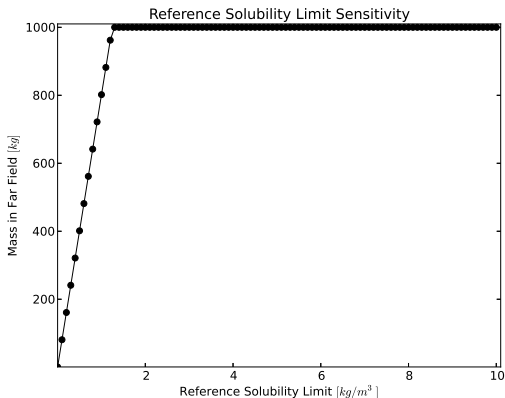


Figure 21 : Sensitivity demonstration of solubility limitation in CYDER for an arbitrary isotope assigned a variable solubility limit.



## Specific Temperature Change Calculations

A reference data set of temperature change curves was calculated. Repeated runs of a detailed model ([15, 13, 12]) over the range of values in Table 4 determined Specific Temperature Change (STC) values over that range.

Thermal Cases

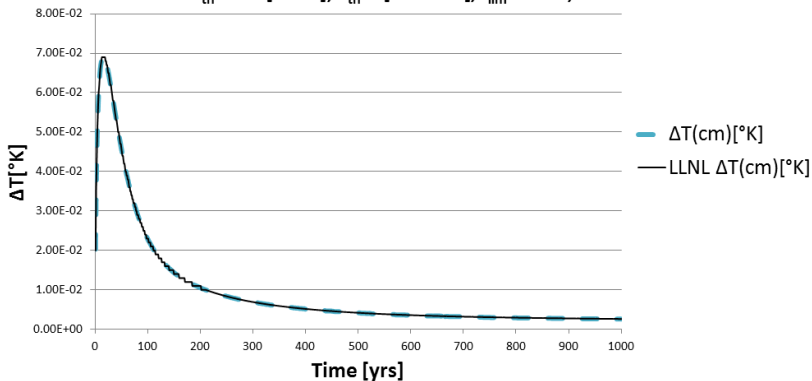
Parameter	Symbol	Units	Value Range
Diffusivity	$\alpha_{th}$	$[m^2 \cdot s^{-1}]$	$1.0 \times 10^{-7} - 3.0 \times 10^{-6}$
Conductivity	$K_{th}$	$[W \cdot m^{-1} \cdot K^{-1}]$	0.1 – 4.5
Spacing	$S$	$[m]$	2, 5, 10, 15, 20, 25, 50
Radius	$r_{lim}$	$[m]$	0.1, 0.25, 0.5, 1, 2, 5
Isotope	$i$	$[-]$	<sup>241,243</sup> Am, <sup>242,243,244,245,246</sup> Cm, <sup>238,240,241,242</sup> Pu, <sup>134,135,137</sup> Cs <sup>90</sup> Sr

**Table 3 :** A thermal reference dataset of STC values as a function of each of these parameters was generated by repeated parameterized runs of the LLNL MathCAD model[12, 13].



## Thermal Base Case Demonstration

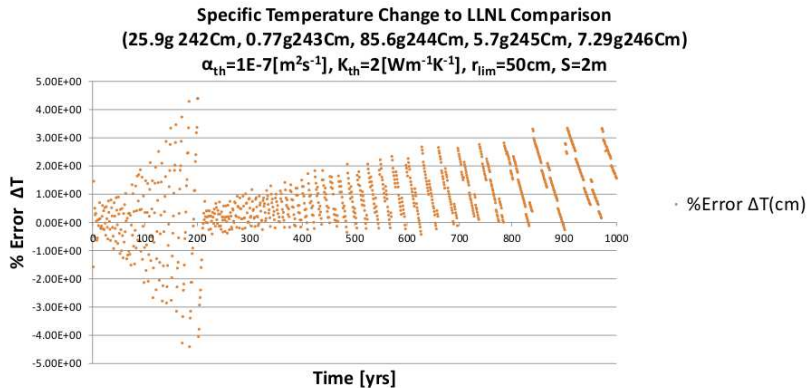
**Specific Temperature Change to LLNL Comparison**  
**(25.9g 242Cm, 0.77g 243Cm, 85.6g 244Cm, 5.7g 245Cm, 7.29g 246Cm)**  
 $\alpha_{th}=1E-7[m^2s^{-1}]$ ,  $K_{th}=2[Wm^{-1}K^{-1}]$ ,  $r_{lim}=50cm$ ,  $S=2m$



**Figure 22 :** This comparison of STC calculated thermal response from  $Cm$  inventory per MTHM in 51GWd burnup UOX PWR fuel compares favorably with results from the semi-analytic model from LLNL



## Thermal Base Case Demonstration

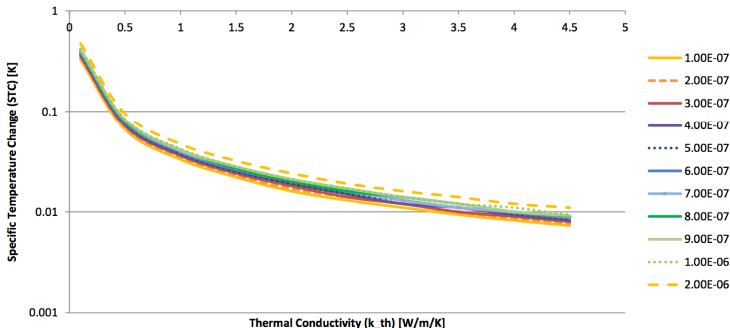


**Figure 23 :** Percent error between the semi-analytic model from LLNL and the STC calculated thermal response from  $Cm$  inventory per MTHM in 51GWd burnup UOX PWR fuel demonstrates a maximum percent error of 4.4%.



## LLNL Model Thermal Conductivity Sensitivity

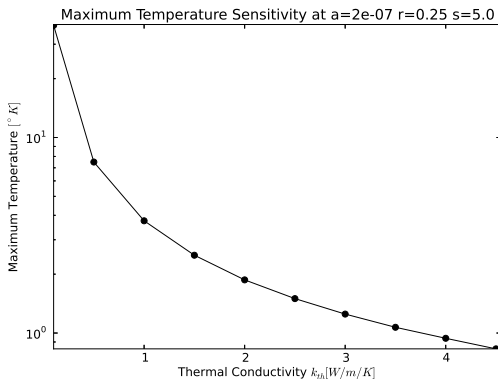
**Thermal Conductivity Sensitivity, LLNL Model Results,  
 $t=30y$ ,  $s=25m$ ,  $r_{lim}=50cm$ , 1kg Cm242 + Daughters**



**Figure 24 :** Increased thermal conductivity decreases the temperature (here represented by STC) at the limiting radius.



## Cyder Thermal Conductivity Sensitivity



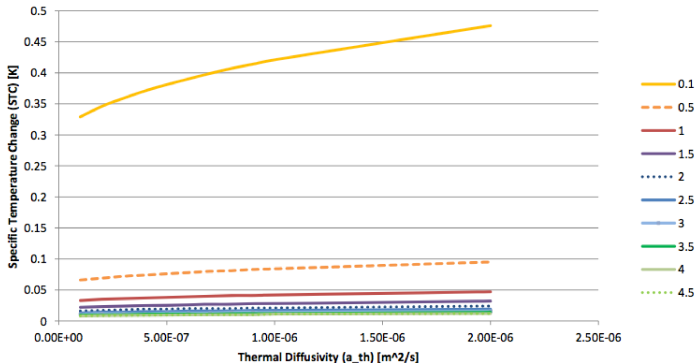
**Figure 25 :** Cyder results agree with those of the LLNL model. Increased  $K_{th}$  decreases temperature change at the limiting radius. The above example thermal profile results from 10kg of  $^{242}\text{Cm}$ ,  $\alpha_{th} = 2 \times 10^{-7}$ ,  $s = 5m$ , and  $r_{lim} = 0.25m$ .





## LLNL Model Thermal Diffusivity Sensitivity

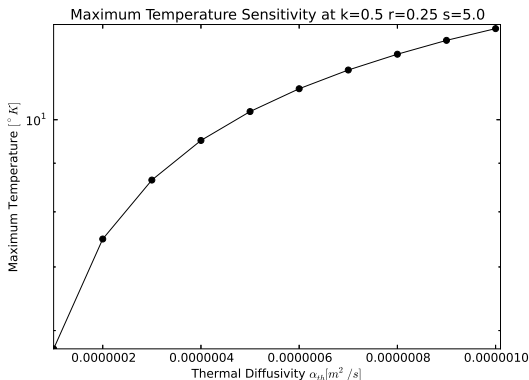
**Thermal Diffusivity Sensitivity, LLNL Model Results,  
 $t=30$  y,  $s=25$ m,  $r_{lim}=50$ cm, 1kg Cm242 + Daughters**



**Figure 26 :** Increased thermal diffusivity decreases temperature change (here represented by STC) at the limiting radius (here  $r_{calc} = 0.5m$ ).



## Cyder Thermal Diffusivity Sensitivity



**Figure 27 :** Cyder trends agree with those of the LLNL model, in which increased thermal diffusivity results in reduced temperature change at the limiting radius. The above example thermal profile results from 10kg of  $^{242}Cm$ .



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## ③ Conclusion



## Conclusion : Summary of Contributions

This work has provided a software platform capable of bridging the gap between fuel cycle simulation and repository performance analysis.

- Conducted thermal transport sensitivity analyses. [19, 18]
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- CYDER achieved integration with a fuel cycle simulator.
- Abstracted physical models of thermal and contaminant transport. [22]
- Demonstrated dominant physics of those models in CYDER, integrated with CYCLUS. [23, 17]
- Published source code, documentation, and testing to facilitate extension by external developers. [21]



## Conclusion : Suggested Future Work

Further work could include

- cultivation of a developer community,
- more detailed benchmarking validation against sophisticated tools,
- comparison against experimental data, where available,
- demonstration of dynamic fuel cycle feedback sensitivities,
- additional physics (fracture models, biosphere models),
- and additional supporting data.



## Acknowledgements

This work was carried out with the generous support of the **UFD Campaign** at **Argonne National Laboratory**. This work is supported by the U.S. Department of Energy, Basic Energy Sciences, Office of Nuclear Energy, under contract # DE-AC02-06CH11357.



**Figure 28 :** This work relied on CYCLUS, the next generation fuel cycle simulator, and its team. [cylus.github.com](https://cylus.github.com)



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## GDSM Model Advective Diffusive Sensitivity

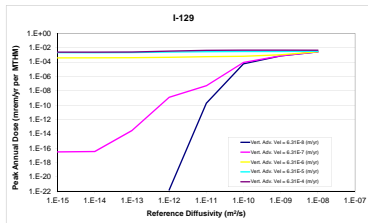


Figure 29 :  $^{129}\text{I}$  reference diffusivity sensitivity.

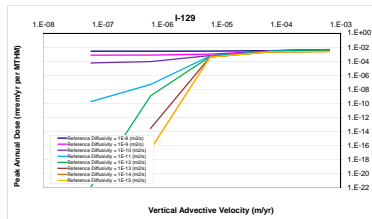
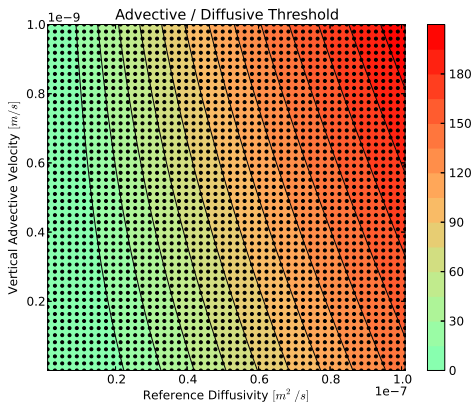


Figure 30 :  $^{129}\text{I}$  vertical advective velocity sensitivity.





## Cyder Advective Diffusive Sensitivity



**Figure 31 :** Dual advective velocity and reference diffusivity sensitivity for a non-sorbing, infinitely soluble nuclide. This demonstration utilized the Degradation Rate model and the coupled advective dispersive mass transfer mode.



# Outline

- 4 Thermal Methodology
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Analytical Model Background
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## Thermal Modeling in Cyder

Two types of thermal modeling occur in Cyder.

- The first is **capacity estimation** for waste stream acceptance.
- The next is **heat evolution** which determines heat evolution in the modules over repository lifetime.



## Thermal Modeling in Cyder

Each can be achieved with one thermal model,

- This model employs a Specific Temperature Change algorithm [30, 29] and
- relies on a supporting **response database** combining detailed spent nuclear fuel composition data [8] with a detailed thermal repository performance analysis tool from Lawrence Livermore National Lab (LLNL) and the Used Fuel Disposition (UFD) campaign [12].
- This method is capable of rapid estimation of temperature increase near emplacement tunnels as a function of
  - waste composition,
  - limiting radius,  $r_{lim}$ ,
  - waste package spacing,  $S$ ,
  - near field thermal conductivity,  $K_{th}$ ,
  - and near field thermal diffusivity,  $\alpha_{th}$ .



## Specific Temperature Change Method

Introduced by Radel, Wilson et al., the Specific Temperature Change (STC) method uses a linear approximation to arrive at the thermal loading density limit [29, 30].

First,  $\Delta T$  is determined for a limiting loading density of the particular material composition then it is normalized to a single kilogram of that material,  $\Delta t$ , the so called STC.

$$\Delta T(r_{lim}) = m \cdot \Delta t(r_{lim}) \quad (4)$$

where

$\Delta T$  = Temperature change due to  $m$  [K]

$m$  = Mass of heat generating material [kg]

$\Delta t$  = Temperature change due to 1 kg [K/kg]

$r_{lim}$  = Limiting radius [m].



## Specific Temperature Change Superposition

For an arbitrary waste stream composition, scaled curves,  $\Delta t_i$ , calculated in this manner for individual isotopes can be superimposed for each isotope to arrive at an approximate total temperature change.

$$\Delta T(r_{lim}) \sim \sum_i m_i \Delta t_i(r_{lim}) \quad (5)$$

where

- $i$  = An isotope in the material [—]
- $m_i$  = mass of isotope  $i$  [kg]
- $\Delta t_i$  = Specific temperature change due to  $i$  [K].



## LLNL UFD MathCAD Model

The analytic model used to populate the reference dataset was created at LLNL for the UFD campaign [15, 13, 12]. It employs an analytic model from Carslaw and Jaeger and is **implemented in MathCAD** [7, 28]. The integral solver in the MathCAD toolset is the primary calculation engine for the analytic MathCAD thermal model, which relies on superposition of point, finite-line, and line source integral solutions.



## Specific Temperature Change Calculations

A reference data set of temperature change curves was calculated. Repeated runs of a detailed model over the range of values in Table 4 determined Specific Temperature Change (STC) values over that range.

Thermal Cases

Parameter	Symbol	Units	Value Range
Diffusivity	$\alpha_{th}$	$[m^2 \cdot s^{-1}]$	$1.0 \times 10^{-7} - 3.0 \times 10^{-6}$
Conductivity	$K_{th}$	$[W \cdot m^{-1} \cdot K^{-1}]$	0.1 – 4.5
Spacing	$S$	$[m]$	2, 5, 10, 15, 20, 25, 50
Radius	$r_{lim}$	$[m]$	0.1, 0.25, 0.5, 1, 2, 5
Isotope	$i$	$[-]$	<sup>241,243</sup> Am, <sup>242,243,244,245,246</sup> Cm, <sup>238,240,241,242</sup> Pu, <sup>134,135,137</sup> Cs <sup>90</sup> Sr

**Table 4 :** A thermal reference dataset of STC values as a function of each of these parameters was generated by repeated parameterized runs of the LLNL MathCAD model[12, 13].

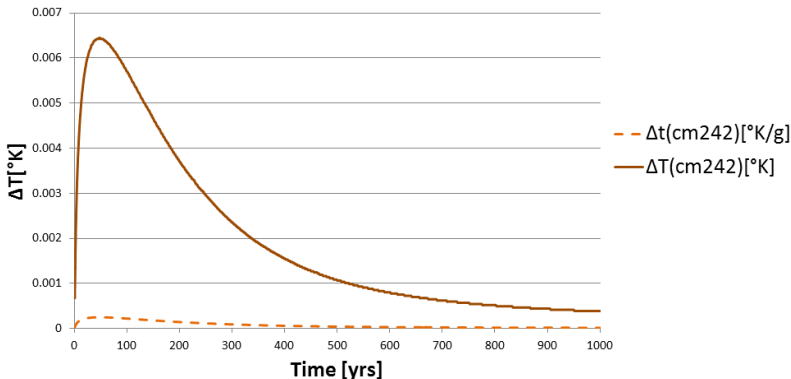




## Scaling Demonstration

### Specific Temperature Change Scaling Calculation (25.9g $^{242}\text{Cm}$ )

$$\alpha_{\text{th}}=1\text{E-}7[\text{m}^2\text{s}^{-1}], K_{\text{th}}=2[\text{Wm}^{-1}\text{K}^{-1}], r_{\text{lim}}=50\text{cm}, S=2\text{m}$$



**Figure 32 :** As a demonstration of the calculation procedure, the temperature change curve for one initial gram of  $^{242}\text{Cm}$  and is scaled to represent 25.9g, approximately the  $^{242}\text{Cm}$  inventory per MTHM in 51GWd burnup LQX PWR fuel



## Superposition Concept

The supporting database was limited to some primary heat contributing isotopes present in traditional spent nuclear fuel,  $H$ , such that the superposition in equation (5) becomes

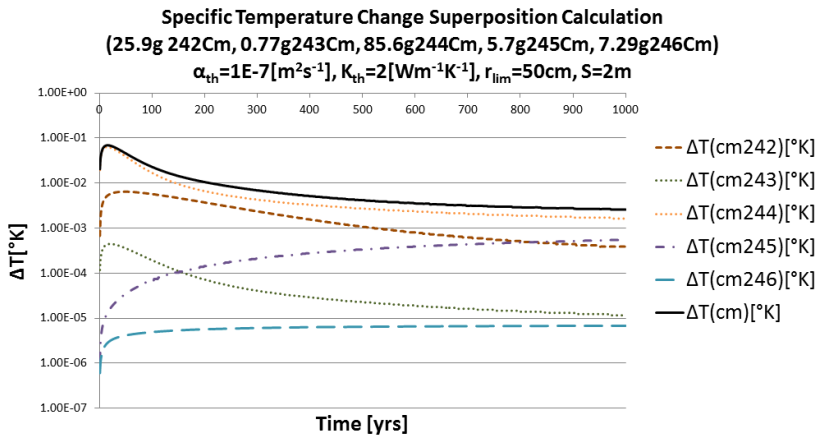
$$\Delta T(r_{lim}, S, K_{th}, \alpha_{th}) \sim \sum_{i \in H} m_i \Delta t_i(r_{lim}, S, K_{th}, \alpha_{th}) \quad (6)$$

where

$$\begin{aligned} H &= \text{set of high heat isotopes } [-] \\ S &= \text{uniform waste package spacing } [m] \\ K_{th} &= \text{thermal conductivity } [W \cdot m^{-1} \cdot K^{-1}] \\ \alpha_{th} &= \text{thermal diffusivity } [m^2 \cdot s^{-1}] \end{aligned} \quad (7)$$



## Superposition Demonstration



**Figure 33 :** As a demonstration of the calculation procedure, scaled temperature change curves for five curium isotopes are superimposed to achieve a total temperature change (note log scale)



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## Timestepping Algorithm

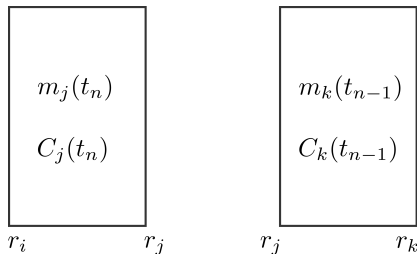
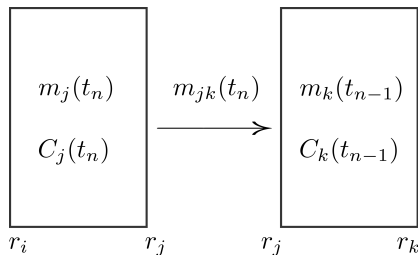


Figure 34 : Two components share an interface at  $r_j$  and contain mass and concentration profiles at the beginning of timestep  $t_n$ .



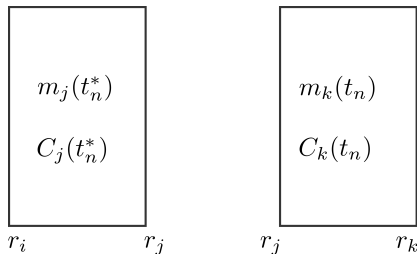
## Timestepping Algorithm



**Figure 35 :** The mass balance model in component k calculates the appropriate mass transfer based on boundary information from component j.



## Timestepping Algorithm



**Figure 36 :** Based on the mass transfer, both components update their mass and concentration profiles based on their mass balance model.



## Advection Dispersion Equation

In a saturated, reducing environment, contaminants are transported by **dispersion** and **advection** [32, 37, 35]:

$$\begin{aligned}
 J &= J_{dis} + J_{adv} \\
 &= -\theta(D_{mdis} + \tau D_m)\nabla C + \theta vC \\
 &= -\theta D \nabla C + \theta vC
 \end{aligned}
 \tag{8}$$

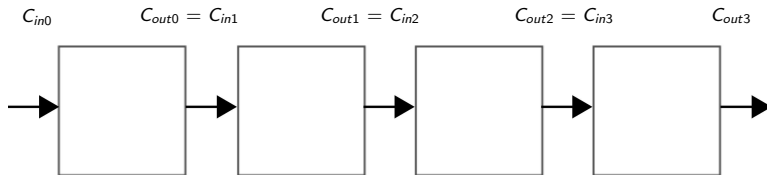
where

$$\begin{aligned}
 J_{dis} &= \text{Total Dispersive Mass Flux } [kg/m^2/s] \\
 J_{adv} &= \text{Advective Mass Flux } [kg/m^2/s] \\
 \tau &= \text{Toruosity } [-] \\
 \theta &= \text{Porosity } [-] \\
 D_m &= \text{Molecular diffusion coefficient } [m^2/s] \\
 D_{mdis} &= \text{Coefficient of mechanical dispersivity} [m^2/s] \\
 D &= \text{Effective Dispersion Coefficient } [m^2/s] \\
 C &= \text{Concentration } [kg/m^3] \\
 v &= \text{Fluid Velocity in the medium } [m/s].
 \end{aligned}$$





## Radionuclide Transport: Lumped Parameter Transport Model



**Figure 37 :** The method by which each lumped parameter component is modeled is according to a relationship between the incoming concentration,  $C_{in}(t)$ , and the outgoing concentration,  $C_{out}(t)$ .

$$C_{out}(t) = \int_0^{\infty} C_{in}(t - t')g(t')e^{-\lambda t'} dt' \quad (9)$$

where

$t'$  = time of entry [s]

$t - t'$  = transit time [s]

$g(t - t')$  = response function, a.k.a. transit time distribution[–]

$\lambda$  = radioactive decay constant[s<sup>-1</sup>].



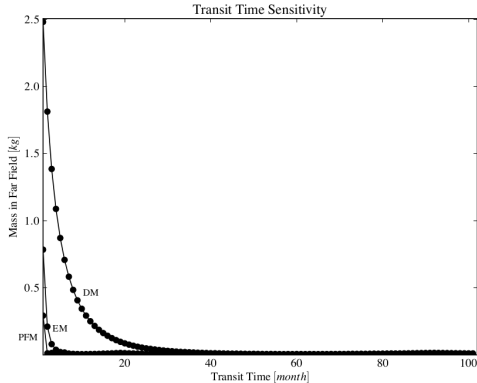
## Radionuclide Transport: Lumped Parameter Transport Model

Some response functions used commonly in chemical engineering applications include the Piston Flow Model (PFM), Exponential Model (EM), and the dispersion model (DM). The solutions to these for constant concentration at the source boundary are given in [25],

$$C(t) = \begin{cases} PFM & C_0 e^{-\lambda t} \\ EM & \frac{C_0}{1 + \lambda t} \\ DM & C_0 e^{\frac{Pe}{2} \left( 1 - \sqrt{1 + \frac{4\lambda t}{Pe}} \right)} \end{cases} \quad (10)$$



## Lumped Parameter Model Base Case



**Figure 38 :** The transit time parameterization of the lumped parameter model has a strong effect on the material reaching the far field after 30 months. The choice of model also strongly affects the results.



## Radionuclide Transport: 1D Finite, Cauchy B.C.

For the boundary conditions,

$$-D \frac{\partial C}{\partial z} \Big|_{z=0} + v_z C = \begin{cases} v_z C_0 & (0 < t < t_0) \\ 0 & (t > t_0) \end{cases} \quad (11)$$

and

$$\frac{\partial C}{\partial z} \Big|_{z=L} = 0 \quad (12)$$

and the initial condition,

$$C(z, 0) = C_i, \quad (13)$$

the solution is given as

$$C(z, t) = \begin{cases} C_i + (C_0 - C_i) A(z, t) & 0 < t \leq t_0 \\ C_i + (C_0 - C_i) A(z, t) - C_0 A(z, t - t_0) & t \geq t_0. \end{cases} \quad (14)$$



## Radionuclide Transport: 1D Finite, Cauchy B.C.

For the vertical flow coordinate system,  $A$  is defined as

$$\begin{aligned}
 A(z, t) = & \left( \frac{1}{2} \right) \operatorname{erfc} \left[ \frac{Rz - vt}{2\sqrt{DRt}} \right] \\
 & + \left( \frac{v^2 t}{\pi RD} \right)^{1/2} \exp \left[ -\frac{(Rz - vt)^2}{4DRt} \right] \\
 & - \frac{1}{2} \left( 1 + \frac{vz}{D} + \frac{v^2 t}{DR} \right) \exp \left[ \frac{vz}{D} \right] \operatorname{erfc} \left[ \frac{Rz + vt}{2\sqrt{DRt}} \right] \\
 & + \left( \frac{4v^2 t}{\pi RD} \right)^{1/2} \left[ 1 + \frac{v}{4D} \left( 2L - z + \frac{vt}{R} \right) \right] \exp \left[ \frac{vL}{D} - \frac{R}{4Dt} \left( 2L - z + \frac{vt}{R} \right)^2 \right] \\
 & - \frac{v}{D} \left[ 2L - z + \frac{3vt}{2R} + \frac{v}{4D} \left( 2L - z + \frac{vt}{R} \right)^2 \right] \exp \left[ \frac{vL}{D} \right] \operatorname{erfc} \left[ \frac{R(2L - z) + vt}{2\sqrt{DRt}} \right]
 \end{aligned}$$

where

$L$  =Extent of the solution domain  $[m]$

$R$  =Retardation factor  $[-]$ .



# Outline

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Analytical Model Background
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## Analytical Model : Background

The analytical model

- was created at LLNL (H. Greenberg, J. Blink, et. al) [15, 13, 12]
- employs an analytic model from Carslaw and Jaeger [7]
- is implemented in MathCAD [28]
- seeks to inform heat limited waste capacity calculations for
  - arbitrary geology
  - arbitrary waste package loading densities
  - arbitrary homogeneous decay heat source



## Analytical Model : Geometry

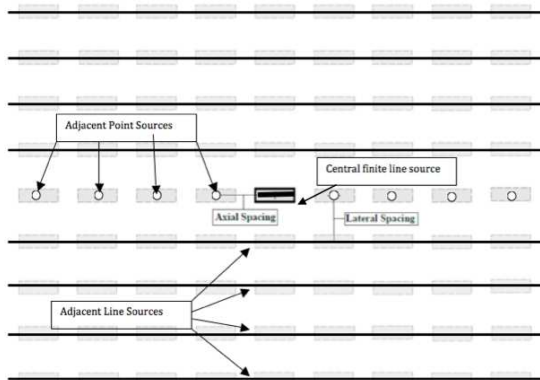


Figure 39 : Vertical, horizontal, alcove, and borehole emplacement layouts can be represented by a line of point sources and adjacent line sources [13].





## Analytical Model : Calculation Method

LLNL's model is a MathCAD solution of the transient homogeneous conduction equation,

$$\nabla^2 T = \frac{1}{\alpha} \frac{\partial T}{\partial t}, \quad (15)$$

in which superimposed point and line source solutions approximate the repository layout.



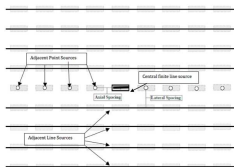
## Analytical Model : Calculation Method

The model consists of two conceptual regions, an external region representing the host rock and an internal region representing the waste form, package, and buffer Engineered Barrier System within the disposal tunnel wall.

- Since the thermal mass of the EBS is small in comparison to the thermal mass of the host rock, the internal region may be treated as quasi-steady state.
- The transient state of the temperature at the calculation radius is found with a convolution of the transient external solution with the steady state internal solution.
- The internal and external regions are **approximated** to be a single homogeneous medium.
- The process is then iterated with a one year resolution in order to arrive at a temperature evolution over the lifetime of the repository.



## Analytical Model : Calculation Method



**Figure 40 :** The central package is represented by a finite line source [13].

The geometric layout of the analytic LLNL model in Figure 42 shows that the central package is represented by the finite line solution

$$T_{line}(t, x, y, z) = \frac{1}{8\pi K_{th}} \int_0^t \frac{q_L(t')}{t-t'} e^{\frac{-(x^2+z^2)}{4\alpha(t-t')}} \cdot \left[ \operatorname{erf} \left[ \frac{1}{2} \frac{(y + \frac{L}{2})}{\sqrt{\alpha(t-t')}} \right] - \operatorname{erf} \left[ \frac{1}{2} \frac{(y - \frac{L}{2})}{\sqrt{\alpha(t-t')}} \right] \right] dt'.$$

(16)



## Analytical Model : Calculation Method

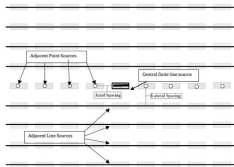


Figure 41 : Adjacent packages are represented as point sources [13].

Adjacent packages within the central tunnel are represented by the point source solution,

$$T_{point}(t, r) = \frac{1}{8K_{th}\sqrt{\alpha\pi}^{\frac{3}{2}}} \int_0^t \frac{q(t')}{(t-t')^{\frac{3}{2}}} e^{\frac{-r^2}{4\alpha(t-t')}} dt'. \quad (17)$$



## Analytical Model : Calculation Method

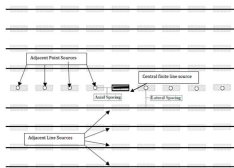


Figure 42 : The non-central disposal tunnels are represented as infinite line sources [13].

Adjacent disposal tunnels are represented by the infinite line source solution,

$$T_{\infty line}(t, x, z) = \frac{1}{4\pi K_{th}} \int_0^t \frac{q_L(t')}{t - t'} e^{-\frac{(x^2+z^2)}{4\alpha(t-t')}} dt' \quad (18)$$

in infinite homogeneous media, where

$\alpha =$  thermal diffusivity [ $m^2 \cdot s^{-1}$ ]

$q(t) =$  point heat source[W]

and

$q_L(t) =$  linear heat source[ $W \cdot m^{-1}$ ]

Superimposed point and line source solutions allow for a notion of the repository layout to be modeled in the host rock.

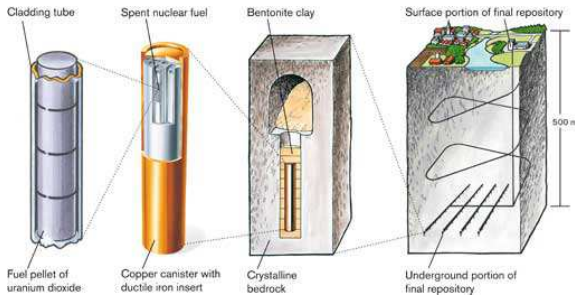


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Analytical Model Background
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## Repository Components



**Figure 43 :** Geologic disposal systems typically employ engineered barrier systems as well as natural barrier systems. This is a Swedish concept in granite [1].



## Clay Disposal Environments

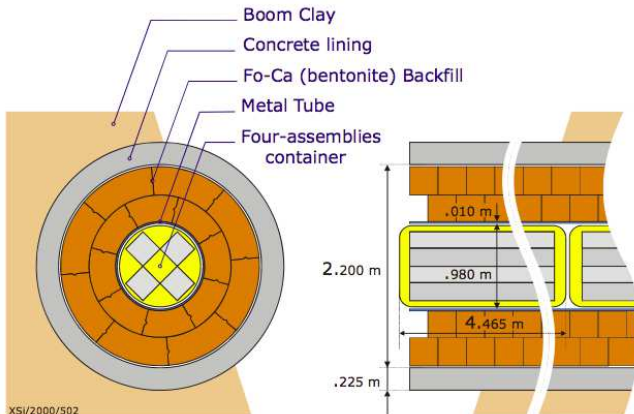


Figure 44 : Belgian reference concept in Boom Clay [36].





## Granite Disposal Environments

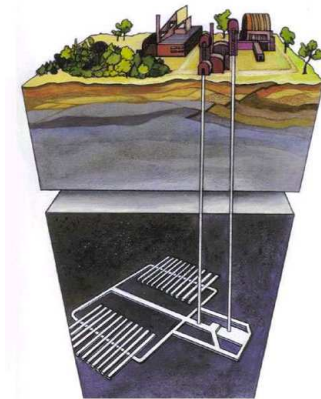


Figure 45 : Czech reference concept in Granite [36].





## Salt Disposal Environments

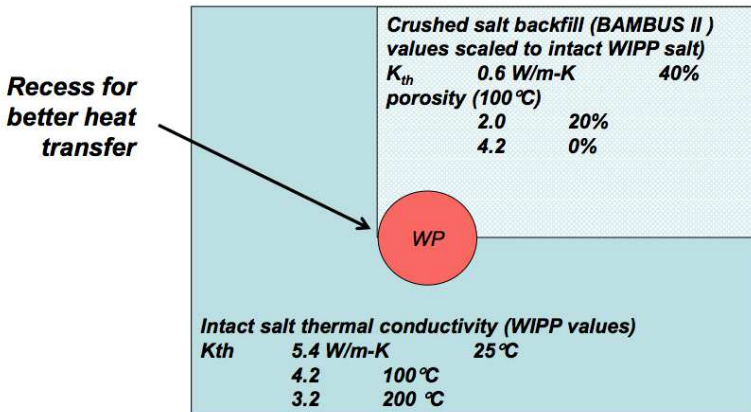


Figure 47 : DOE-NE Used Fuel Disposition Campaign concept in Salt [15].



## Deep Borehole Disposal Environment

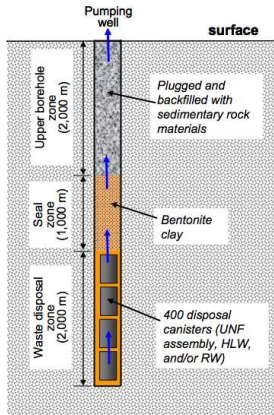


Figure 48 : DOE-NE Used Fuel Disposition Campaign Deep Borehole concept [15].



## Engineered Barriers : Waste Forms

The first line of defense is the waste form.

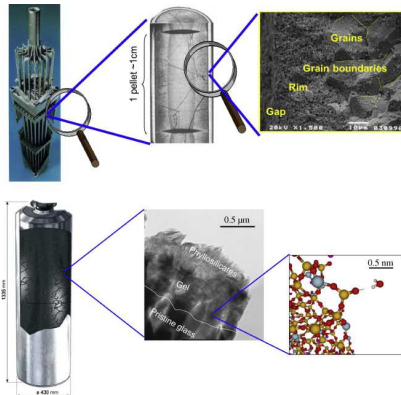


Figure 49 : A comparison of uranium oxide and borosilicate glass waste forms [27].



## Engineered Barriers : Waste Packages

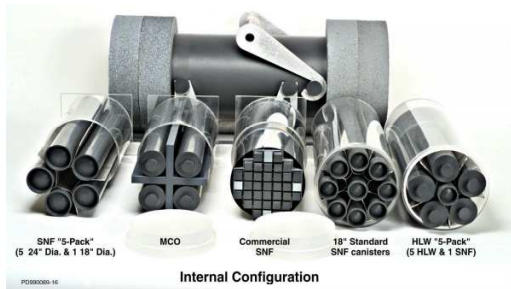


Figure 50 : Conceptual mockup of waste packages around waste forms [5].



## Engineered Barriers : Disposal Cask

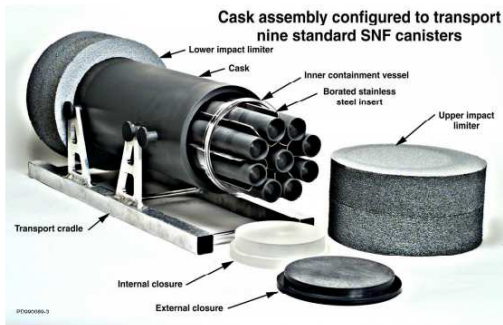


Figure 3. Conceptual design model.

Figure 51 : Conceptual mockup of a transport and disposal cask [5].



## Engineered Barriers : Buffer

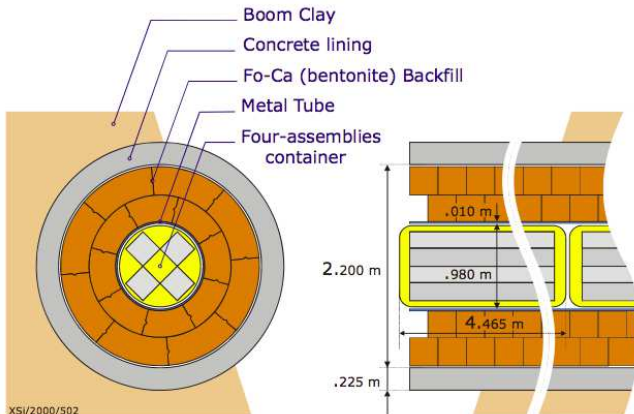
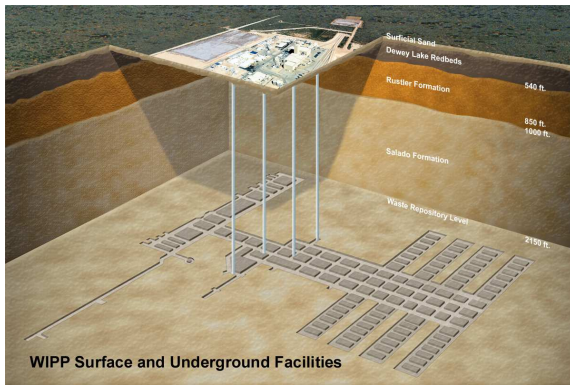


Figure 52 : Belgian reference concept in Boom Clay [36].





## Natural Barrier : Geology

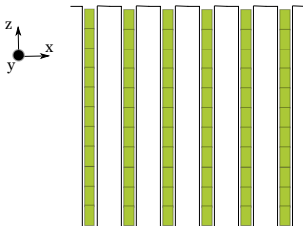


**Figure 53 :** The Waste Isolation Pilot Plant has many geologic layers above the salt bed [10].

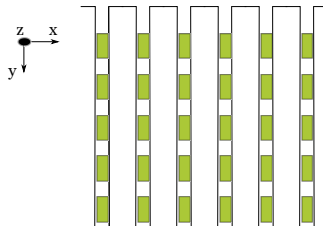


# Repository Layouts

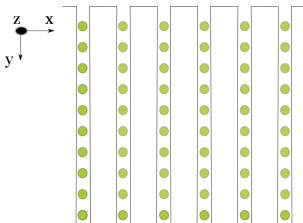
Deep Boreholes



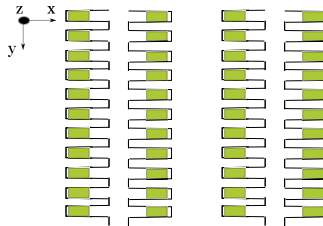
Horizontal In-Tunnel



Vertical In-Tunnel



Alcoves





# Outline

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- ⑥ LLNL Model Background  
Analytical Model Background
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- ⑧ Mixed Cell Model



## Radionuclide Transport : Mixed Cell Sorption

The mass of contaminant sorbed into the degraded and precipitated solids can be found using a linear isotherm model [32], characterized by the relationship

$$s_i = K_{di} c_i \quad (19)$$

where

$s_i$  = the solid concentration of isotope  $i$  [ $kg/kg$ ]

$K_{di}$  = the distribution coefficient of isotope  $i$  [ $m^3/kg$ ]

$c_i$  = the liquid concentration of isotope  $i$  [ $kg/m^3$ ].

From the sorbed contaminant mass, we find the non-sorbed contaminant mass in the free fluid,

$$m_{ffl} = m_{ffT} - \frac{1}{2} \left( m_{ffT} - m_{psm} - \frac{V_{ff}}{K_d} \right) \mp \frac{1}{2} \sqrt{m_{ffT}^2 + 2m_{ffT} \left( m_{psm} - \frac{V_{ff}}{K_d} \right) + \left( m_{psm} + \frac{V_{ff}}{K_d} \right)^2} \quad (20)$$

where

$m_{ffT}$  = total degraded contaminant mass [ $kg$ ]

$m_{psm}$  = noncontaminant mass in degraded and precipitated solids [ $kg$ ]

$m_{psc}$  = contaminant mass in degraded and precipitated solids [ $kg$ ]

$\rho_b$  = bulk (dry) density of the medium [ $kg/m^3$ ].